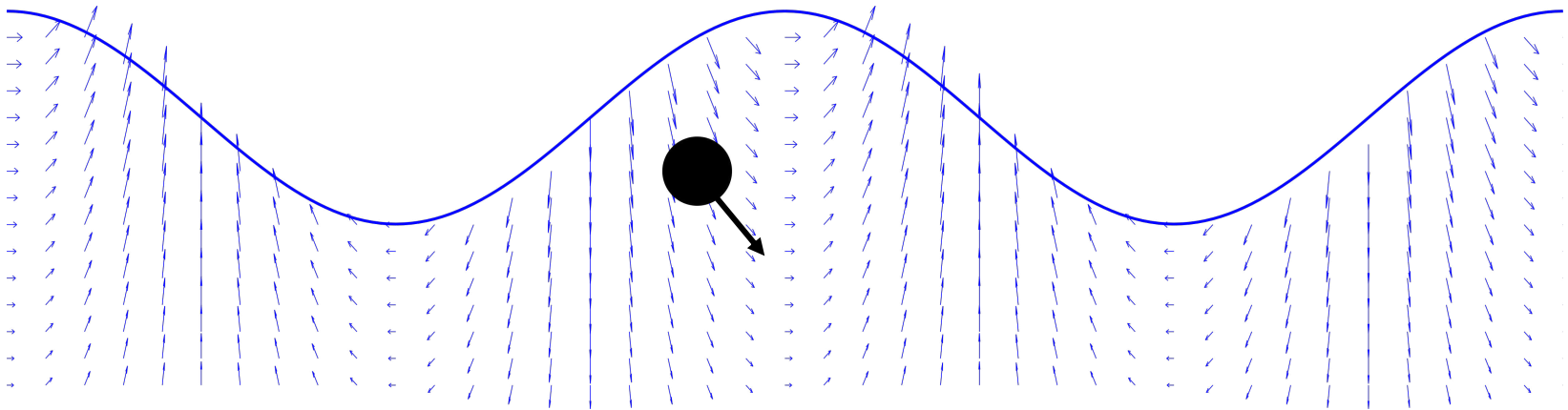


Inertial effects in particle (microplastic) settling through wavy flow

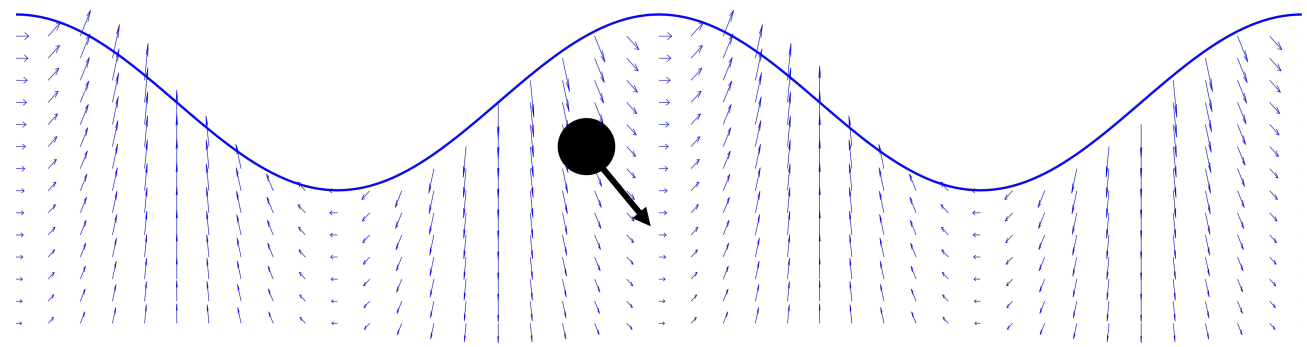


Nimish Pujara



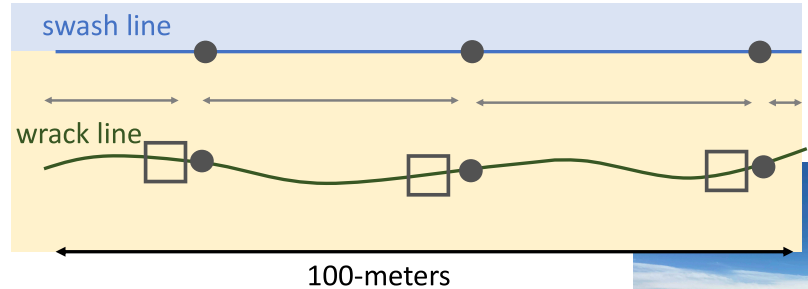
Department of Civil and
Environmental Engineering
UNIVERSITY OF WISCONSIN-MADISON

1. Negatively buoyant particles in surface waves



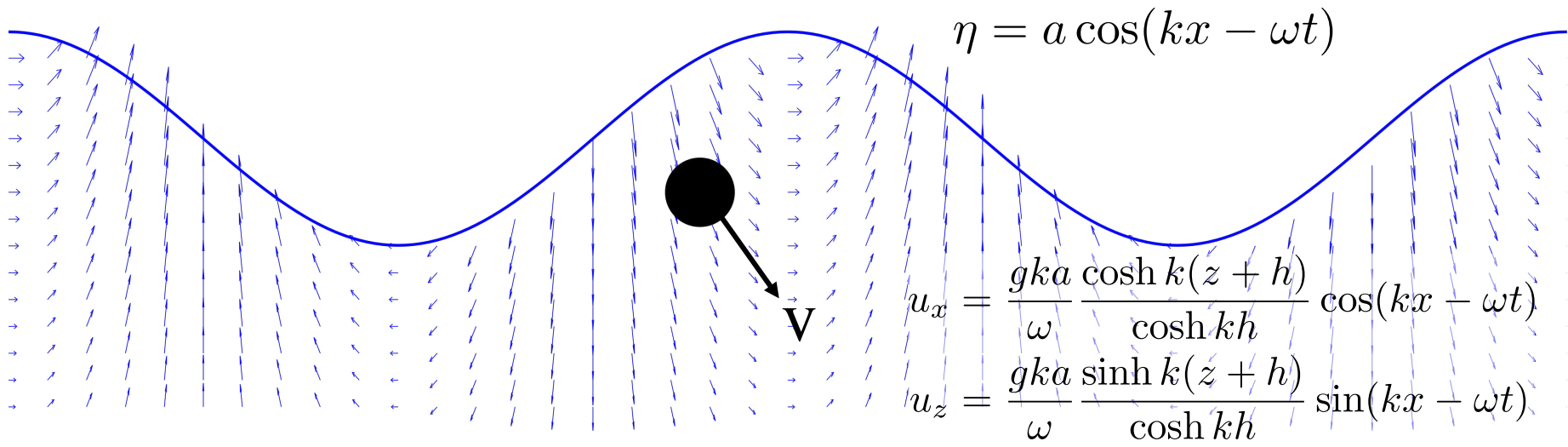
DiBenedetto, M., Clark, L., & Pujara, N. (2022). Enhanced settling and dispersion of inertial particles in surface waves. *Journal of Fluid Mechanics*, 936, A38. doi:10.1017/jfm.2022.95

2. Microplastic beaching and settling in turbulence



- Surface Sample
- Core Sample

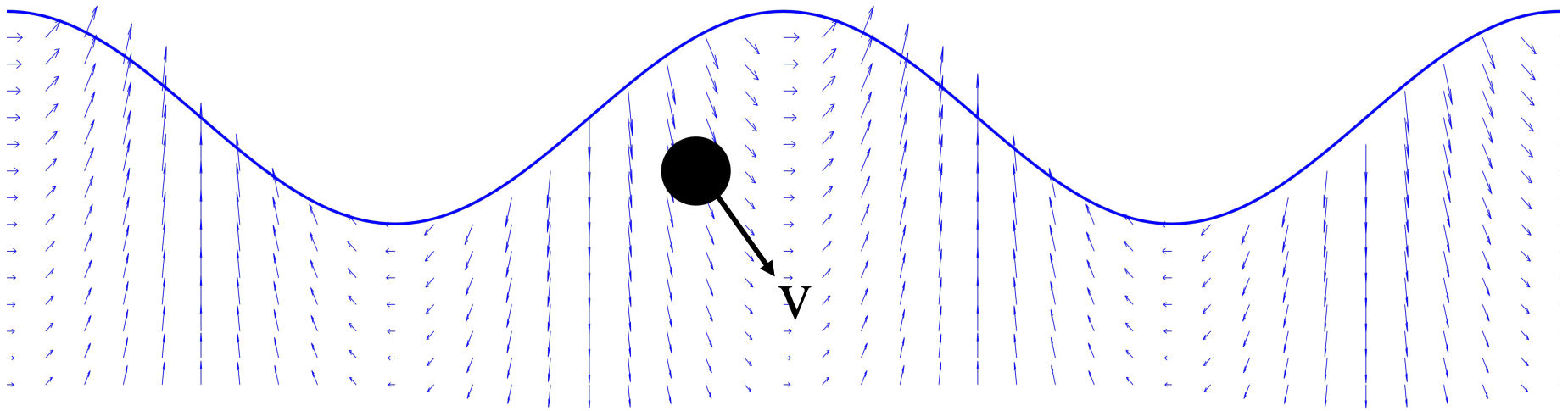




$$m a = \Sigma F$$

$$m_p \frac{dv}{dt} = \underbrace{(m_p - m_f)g}_{\text{buoyancy}} + \underbrace{m_f \frac{Du}{Dt}}_{\text{flow}} - \underbrace{C_m \left[\frac{dv}{dt} - \frac{Du}{Dt} \right]}_{\text{added mass}} - \underbrace{F_{\text{drag}}}_{\text{drag}}$$

Can we predict particle transport without computing numerical solutions of the equation of motion?



Dimensionless equation of motion in linear drag regime ($Re_p \ll 1$)

$$\frac{d\mathbf{v}}{dt} = \frac{(\mathbf{u} - \mathbf{v})}{St} + \beta \frac{D\mathbf{u}}{Dt} - \frac{v_s}{St} \mathbf{e}_z$$

$$St = \omega \tau_p$$

Stokes number

$$\beta = (1 + C_m) / (\gamma + C_m)$$

Fluid forcing coefficient

$$\gamma = m_p / m_f$$

Buoyancy ratio

St number expansion

$$\mathbf{v} = \mathbf{v}_0 + St\mathbf{v}_1 + St^2\mathbf{v}_2 + \dots$$

$$\frac{d\mathbf{v}}{dt} = \frac{(\mathbf{u} - \mathbf{v})}{St} + \beta \frac{D\mathbf{u}}{Dt} - \frac{v_s}{St} \mathbf{e}_z$$

Collect terms at each order

$$\mathbf{v} = \mathbf{u} + \mathbf{v}_s - St(1 - \beta) \frac{D\mathbf{u}}{Dt} + St^2(1 - \beta) \frac{\partial^2 \mathbf{u}}{\partial t^2} + O(\varepsilon^2 St^2, \varepsilon St^3)$$

Evaluate using linear wave theory flow field

$$v_x = A \varepsilon \frac{\cosh z + kh}{\cosh kh} \cos(x - t + \phi) + \varepsilon^2 St(1 - \beta) \frac{\sin 2(x - t)}{2 \cosh^2 kh}$$

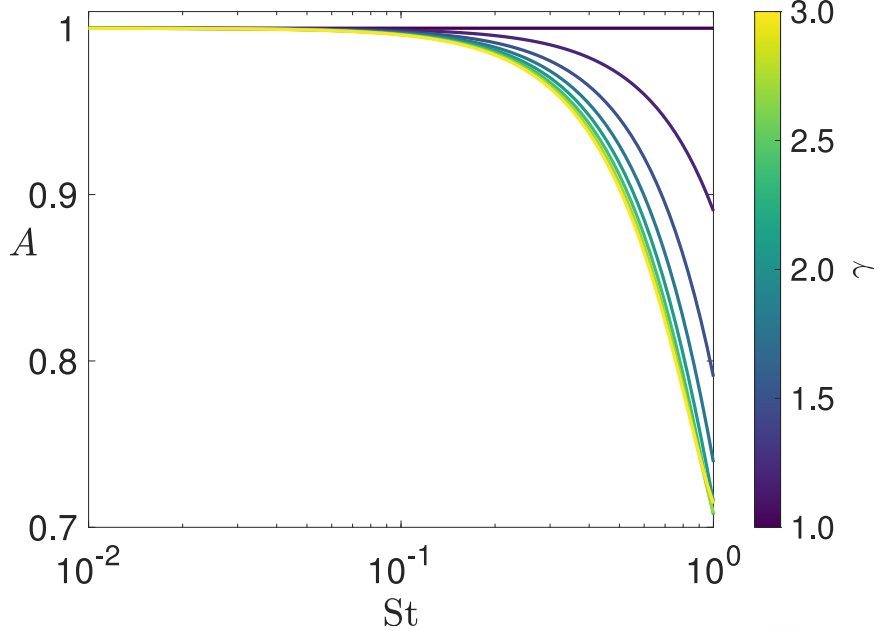
$$v_z = -v_s + A \varepsilon \frac{\sinh z + kh}{\cosh kh} \sin(x - t + \phi) - \varepsilon^2 St(1 - \beta) \frac{\sinh 2(z + kh)}{2 \cosh^2 kh}$$

Fluid flow

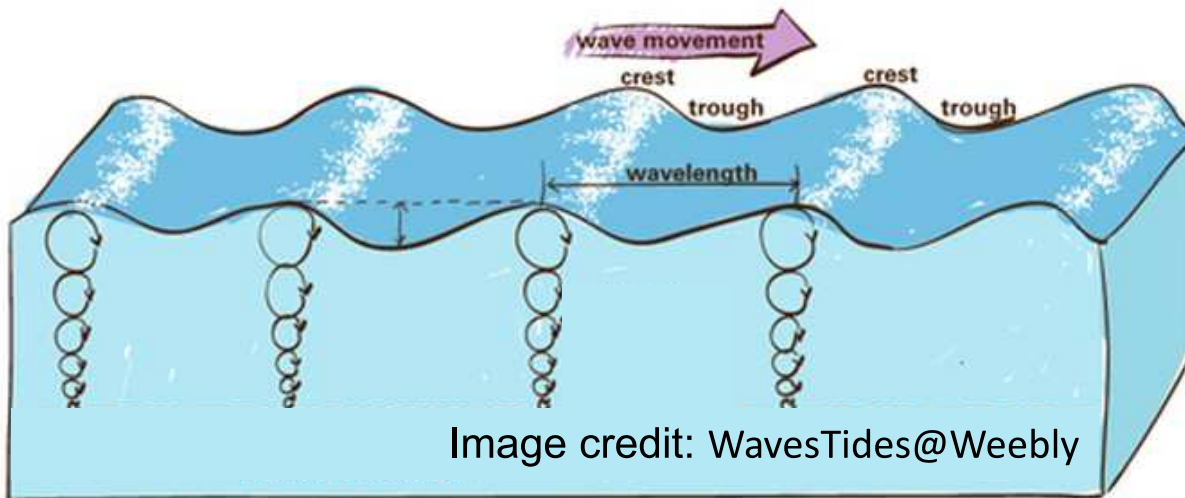
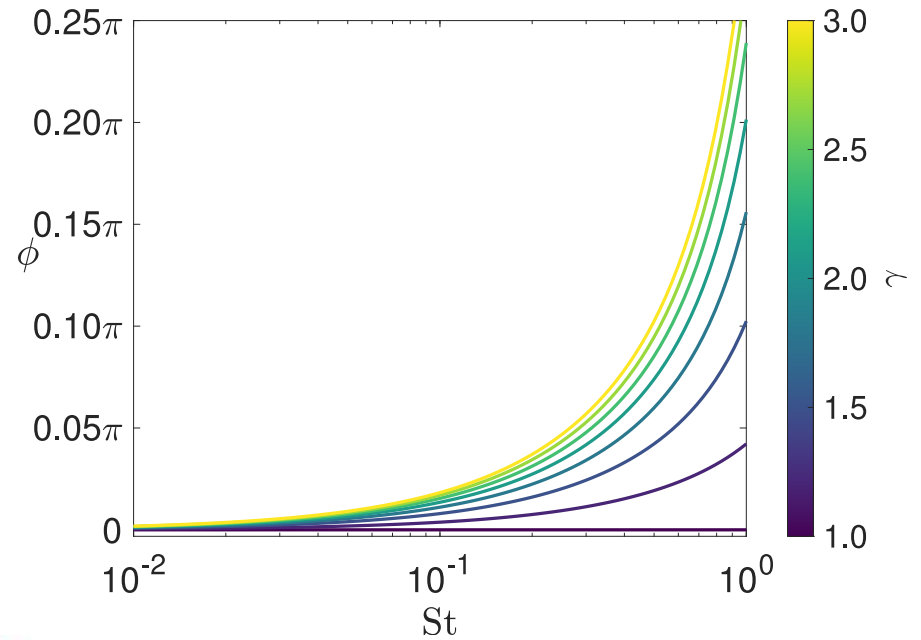
Non-linear wave effects

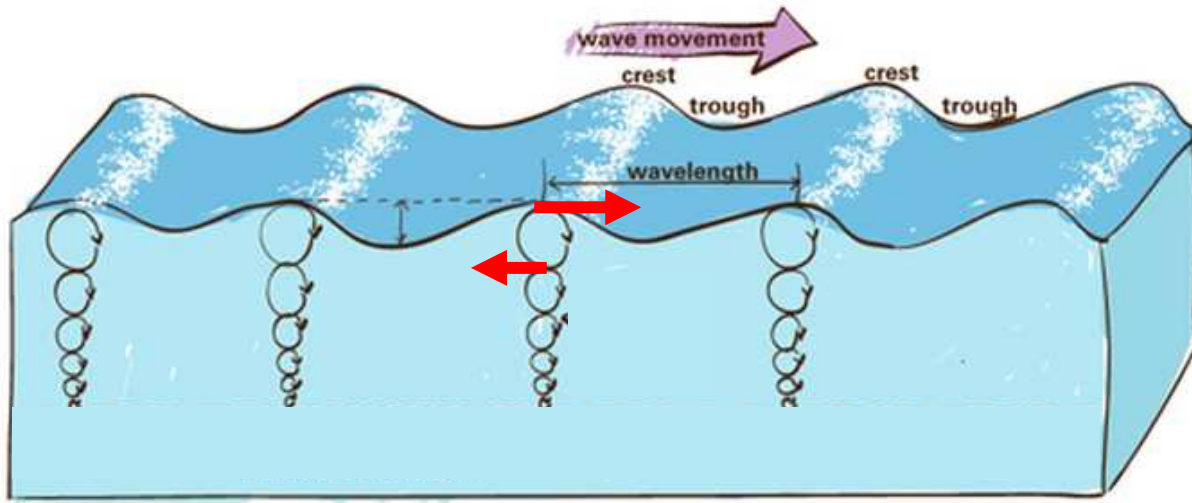
Inertial particle motion

Amplitude

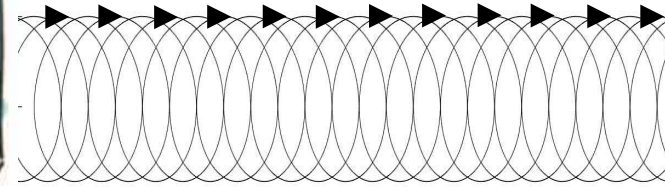


Phase

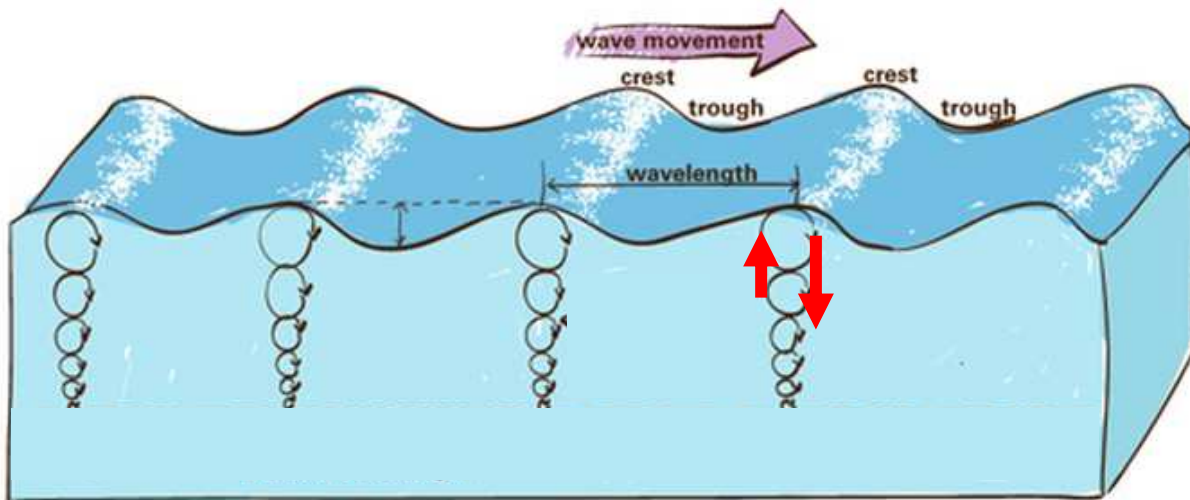




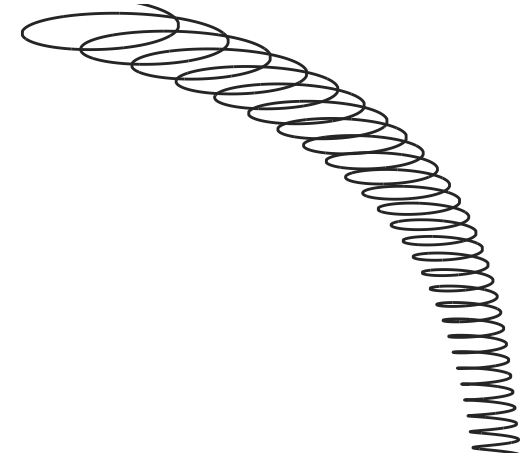
Stokes drift:



Stokes (1847)



Vertical drift:



Eames (2008)
Santamaria et al. (2013)

Multi-timescale expansion

$$\mathbf{x}_p(\tau, T) = \mathbf{x}_{p0}(\tau, T) + \varepsilon \mathbf{x}_{p1}(\tau, T) + \dots \quad \text{where } \tau = t, T = \varepsilon^2 t$$

Substitute into expressions for particle velocity and collect terms at each order. The drifts appear as a solvability condition at second order:

**Reduced
horizontal drift**

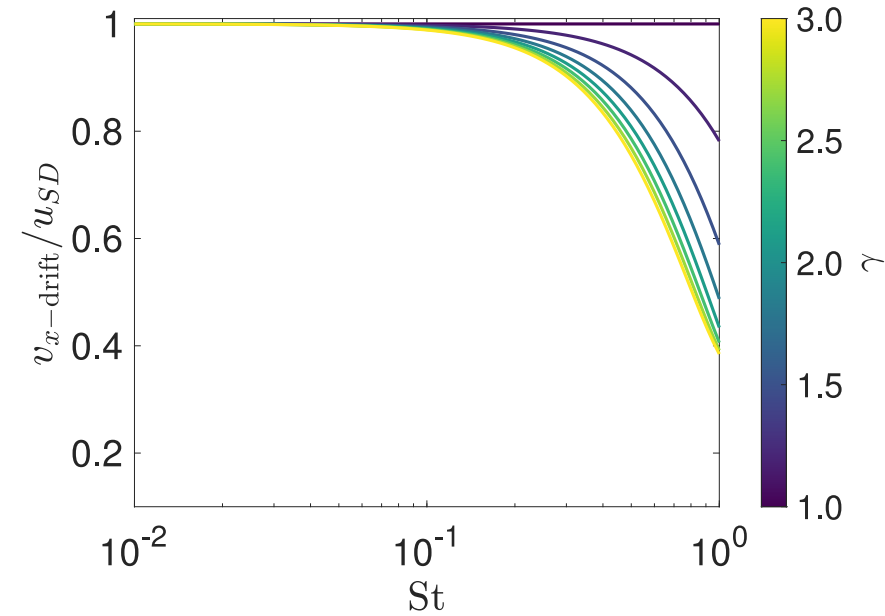
$$v_{x\text{-drift}} = \frac{A^2}{1 + v_s^2} u_{\text{SD}}$$

$$v_{z\text{-drift}} = -v_s \left[1 + \frac{A^2}{1 + v_s^2} u_{\text{SD}} + \frac{1}{2} \tanh kh \frac{du_{\text{SD}}}{dz_{p0}} \right]$$

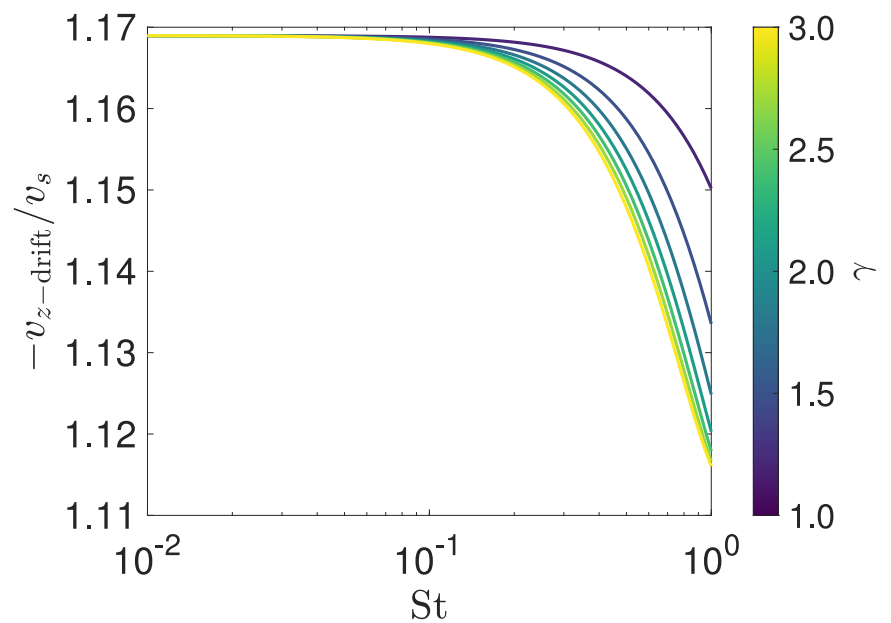
Enhanced settling

Inertial particle drift

Horizontal drift

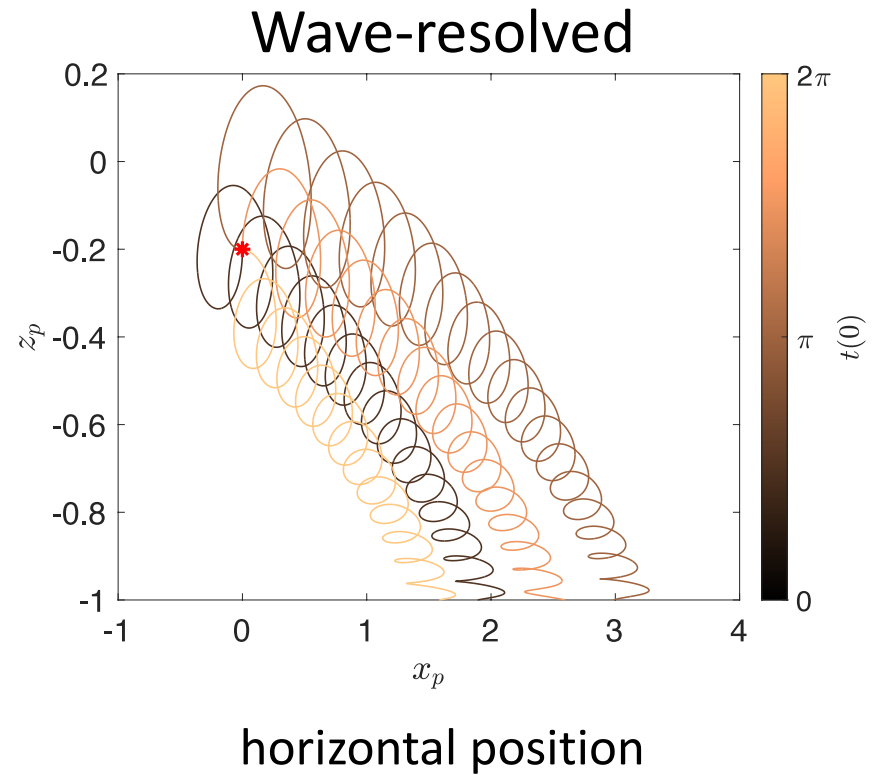
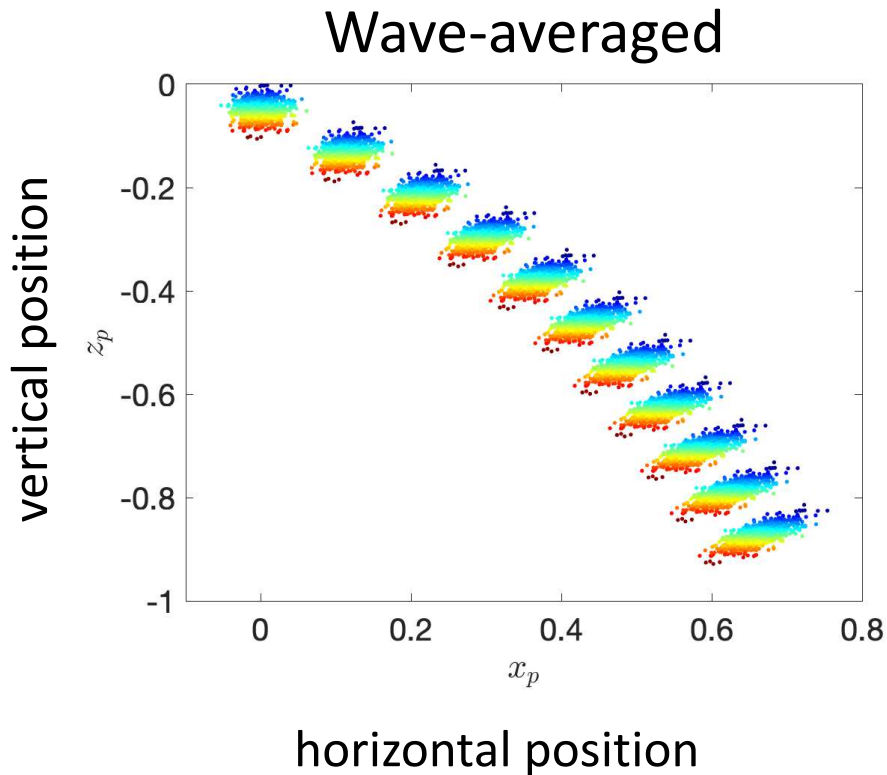


Vertical drift



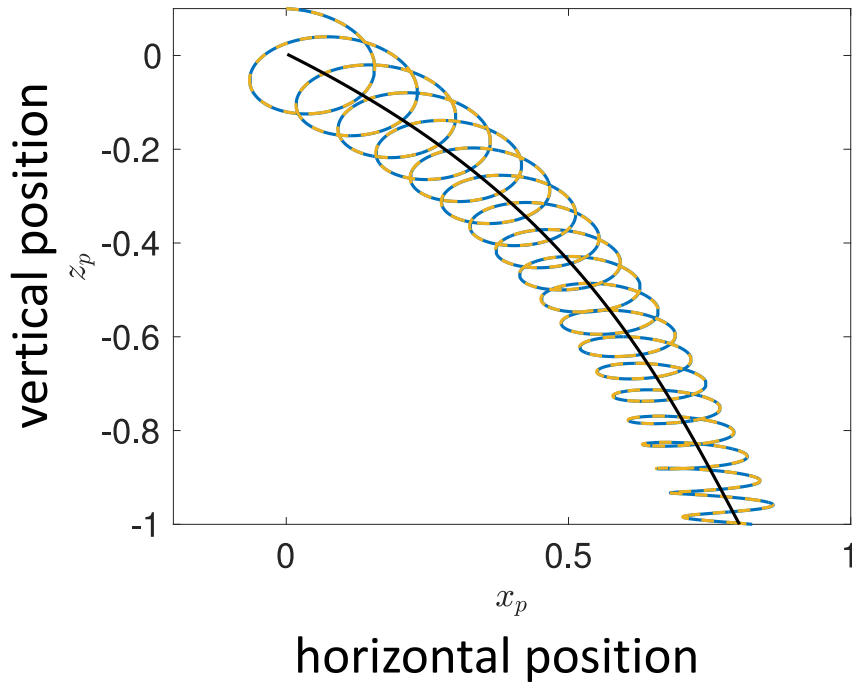
$$\epsilon = 0.33; \quad kh = 1$$

Horizontal dispersion due to vertical shear

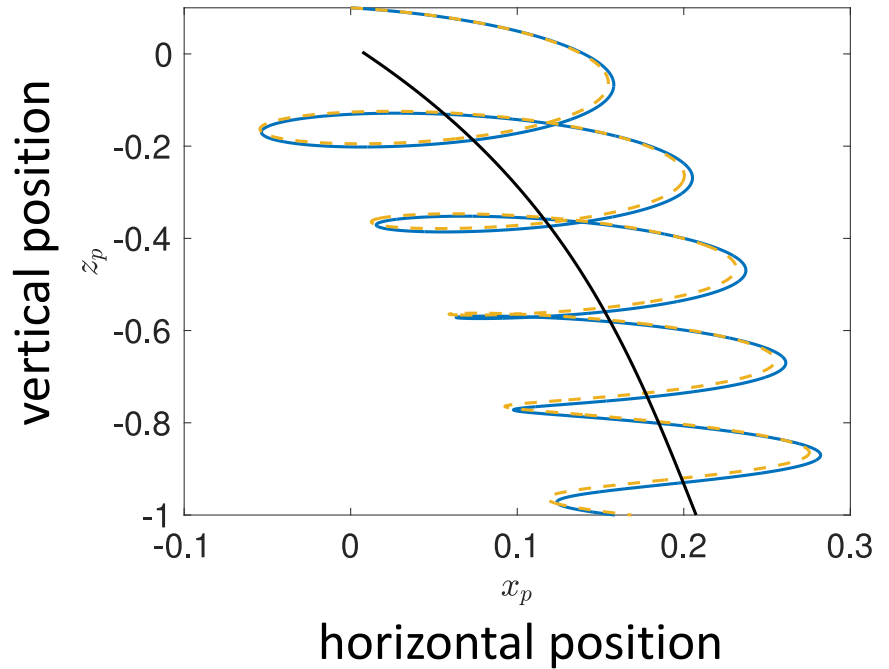


Initial conditions (correctly projected into wave-averaged variables) are important!

Comparison against numerical solutions



$ka = 0.1, kh = 1, \gamma = 1.1, St = 0.1$



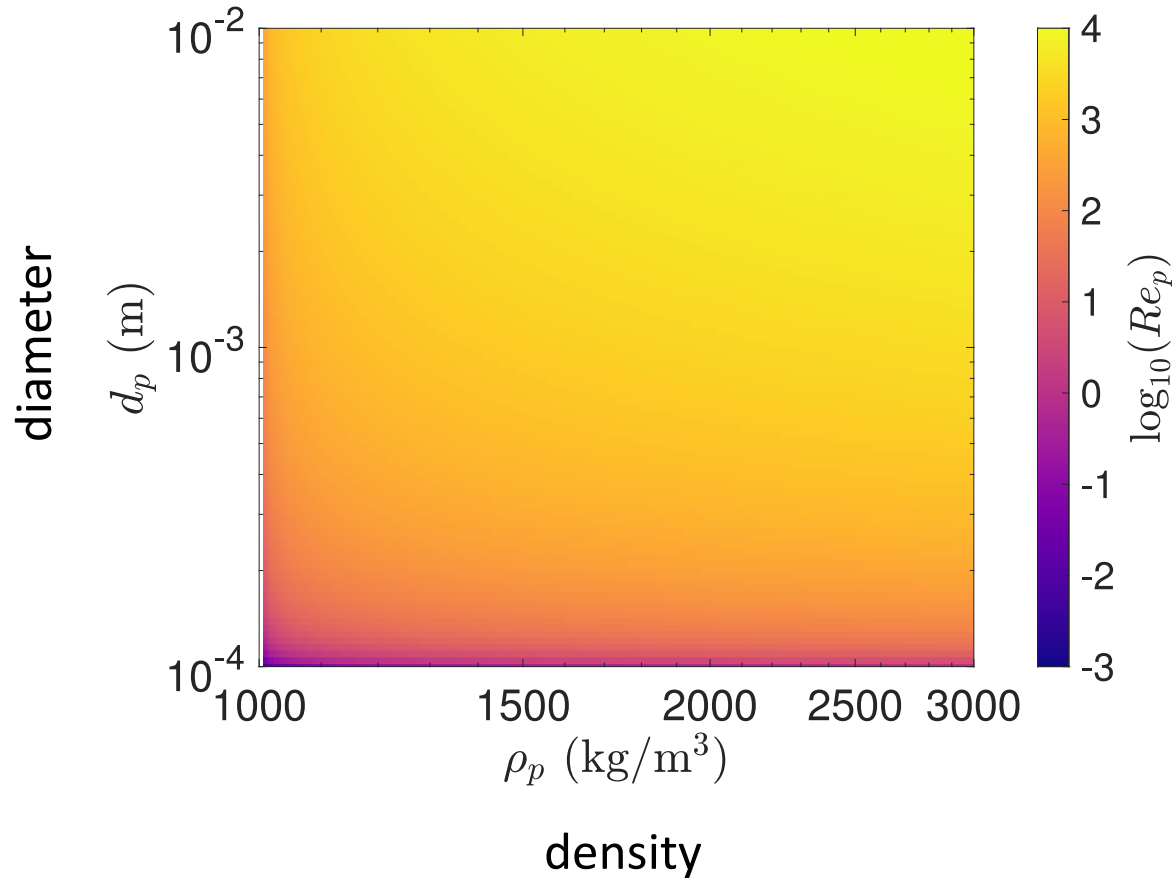
$ka = 0.1, kh = 1, \gamma = 1.05, St = 0.75$

**Numerical
solution**

**Velocity
solution**

**Drift
solution**

Non-linear drag



Microplastics can fall outside the linear (Stokes) drag regime and into the non-linear (intermediate Reynolds number) regime

Non-linear drag

Schiller-Naumann drag model captures the drag in the intermediate Reynolds number regime

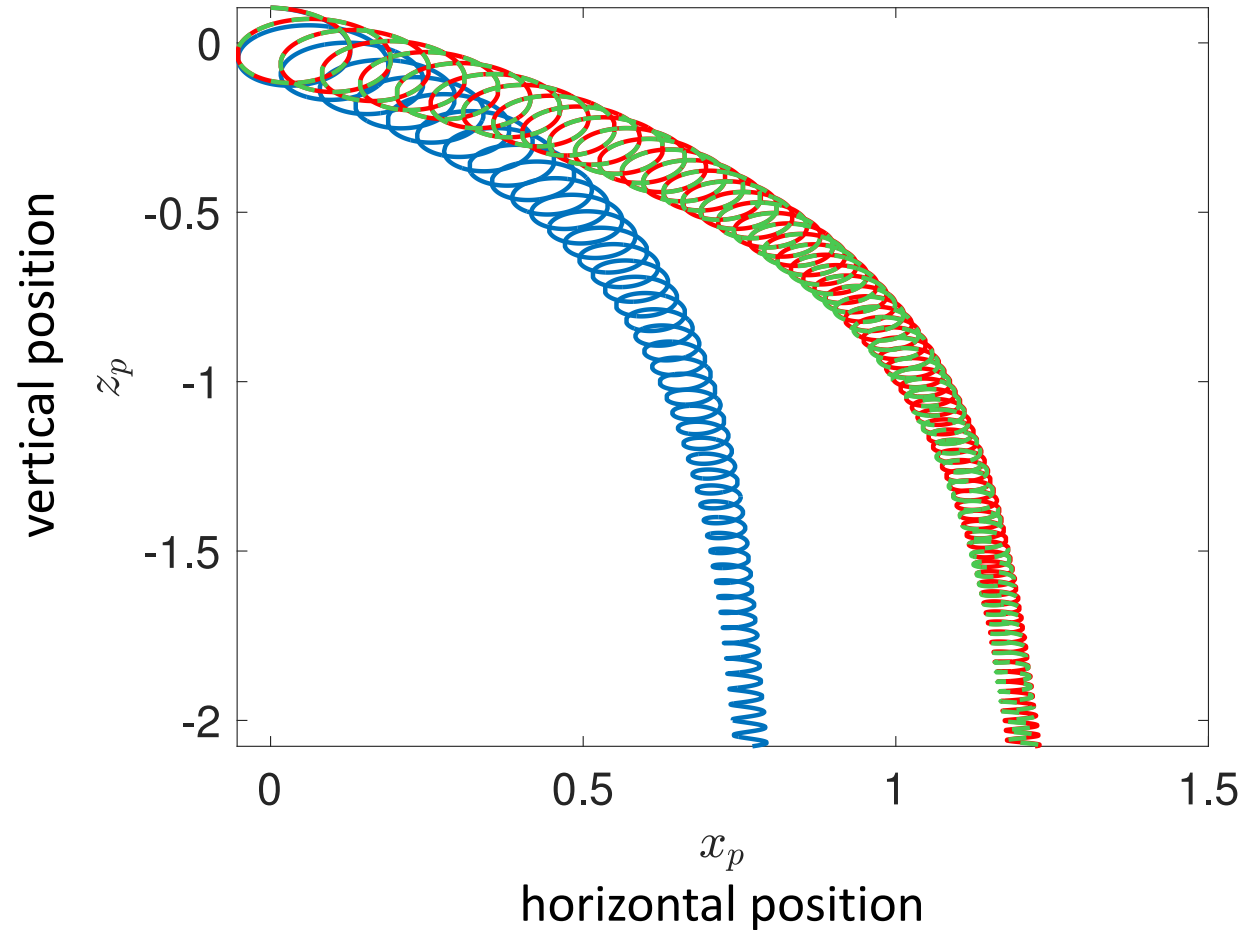
$$C_D = \frac{24}{\text{Re}_p} (1 + 0.15\text{Re}_p^{0.687})$$

Linear drag

“Linearize” the drag model to allow analysis

$$C_D = \frac{24}{\text{Re}_p} (1 + 0.15\text{Re}_{p,t}^{0.687})$$

Non-linear drag

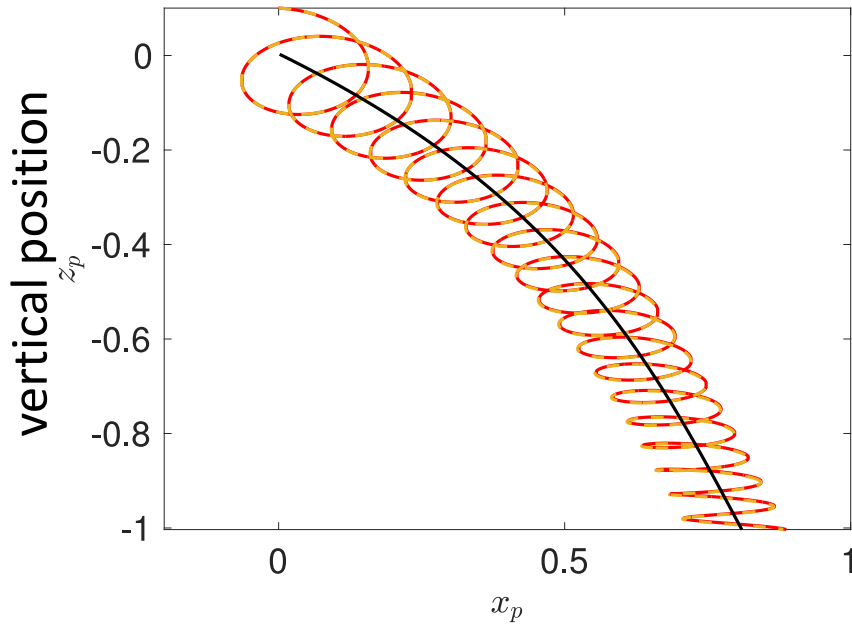


— Stokes drag

— Schiller-Naumann

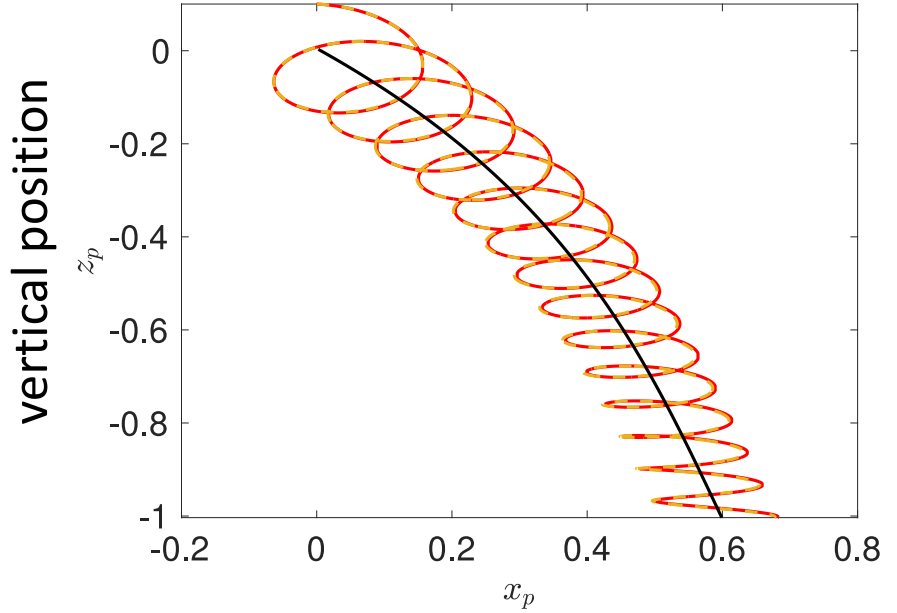
- - - Schiller-Naumann
"Linearized"

Comparison against numerical solutions




horizontal position


$$ka = 0.1, kh = 1, \gamma = 1.1, St_{SN,t} = 0.1, \\ Re_{p,t} = 212$$




horizontal position

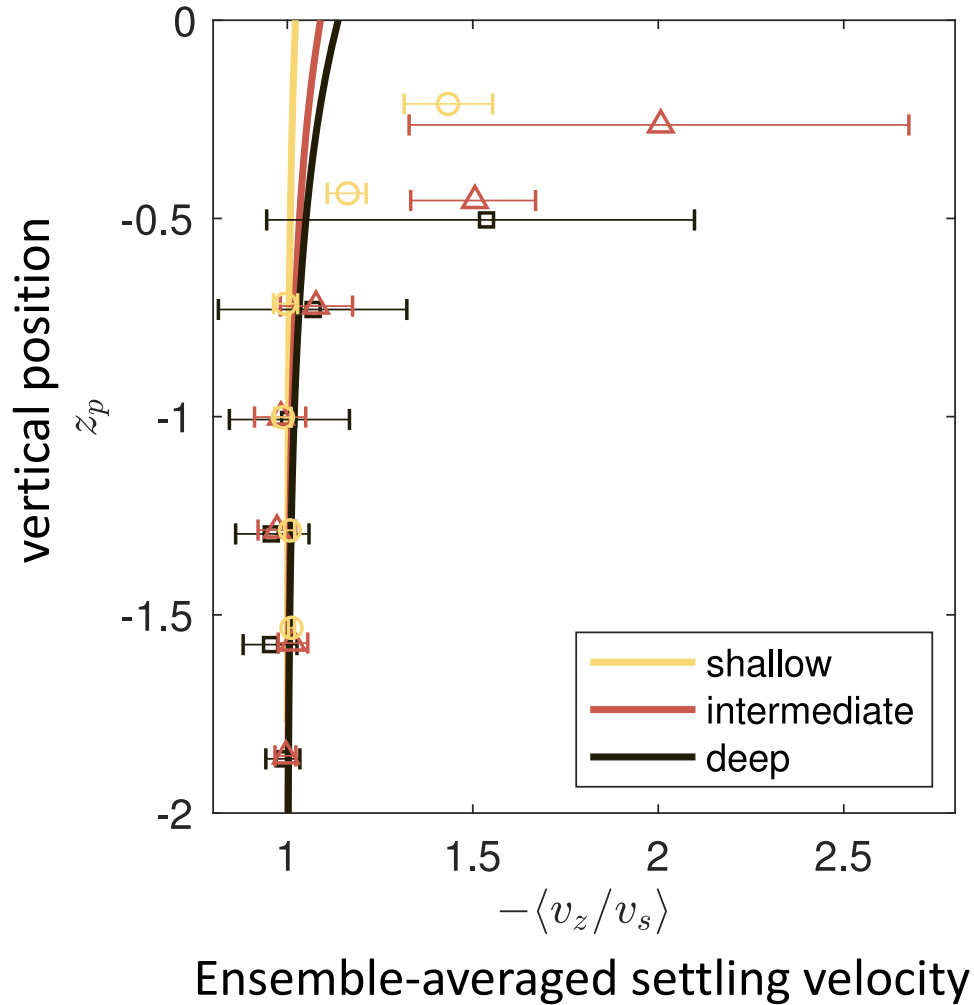
$$ka = 0.1, kh = 1, \gamma = 1.05, St_{SN,t} = 0.5, \\ Re_{p,t} = 1093$$

 Schiller-Naumann
numerical solution

 Velocity solution
“Linearized” drag

 Drift solution
“Linearized” drag

Comparison against laboratory experiments



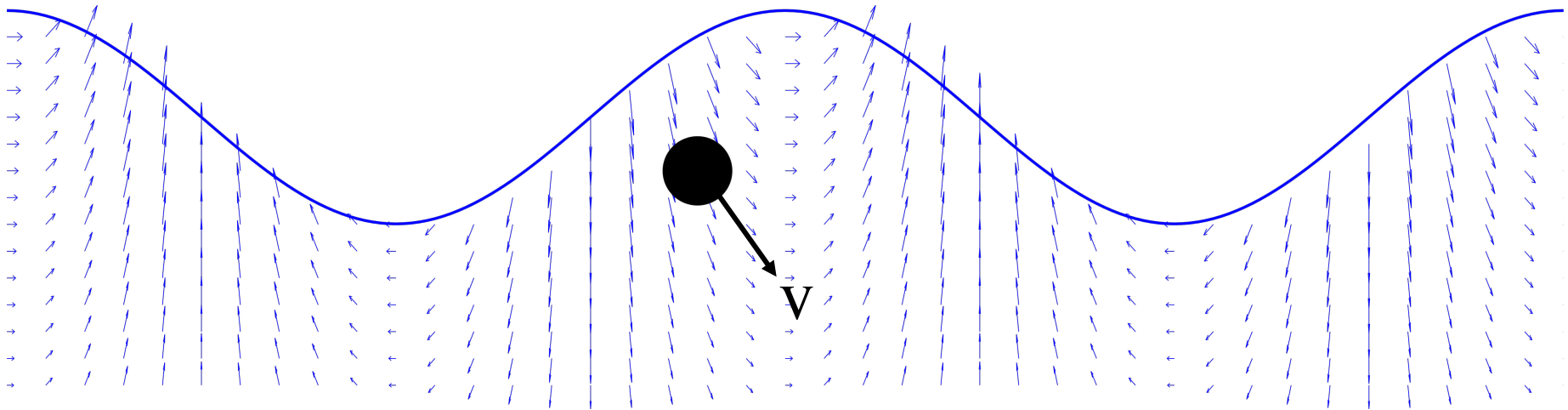
Data from Clark et al. (2020)

Theory captures the trend, if not the full extent of the enhanced settling velocity of inertial particles in surface waves

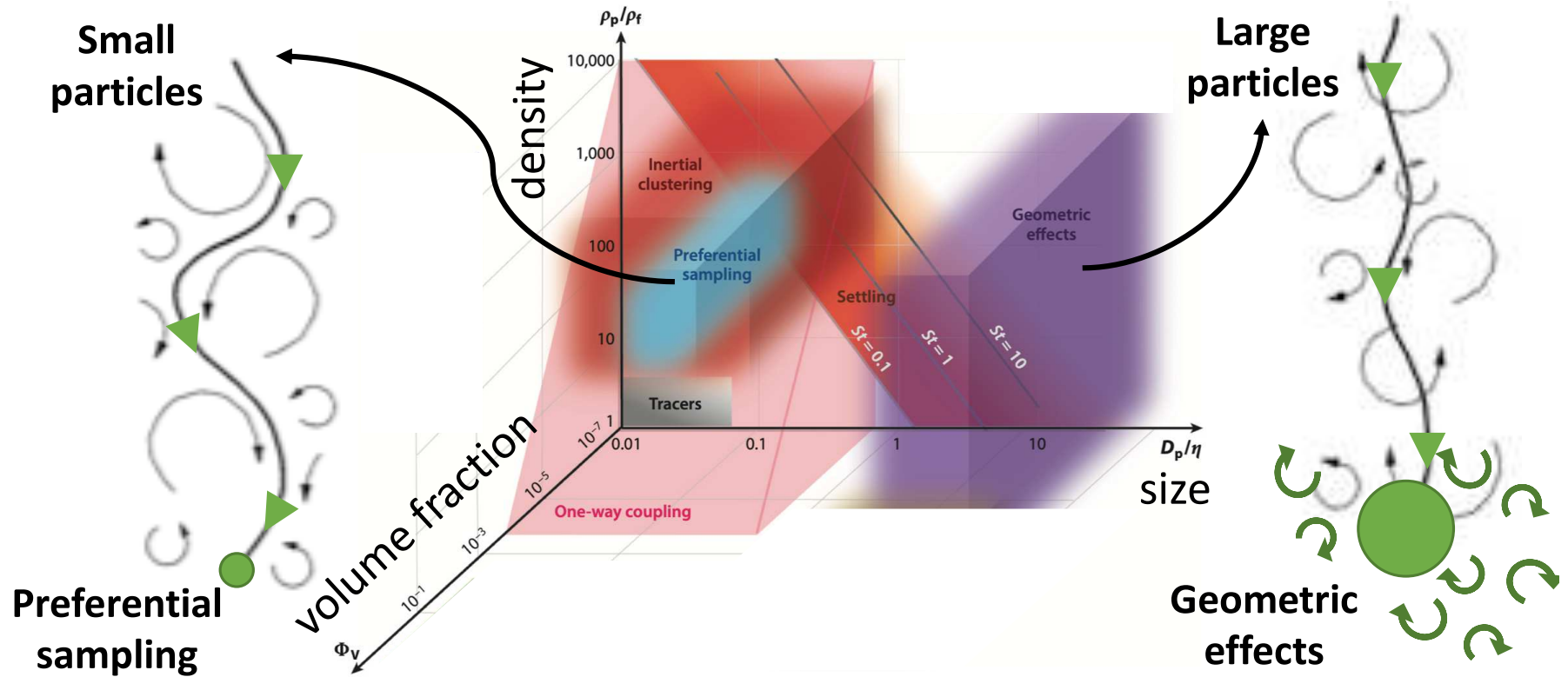
Conclusions

Negatively buoyant particles in surface waves

- Particles trace out small orbitals than fluid particles
- Horizontal drift is reduced relative to fluid particles
- Settling velocity is enhanced relative to terminal settling velocity through dynamical and kinematic (Stokes-drift-like) mechanisms

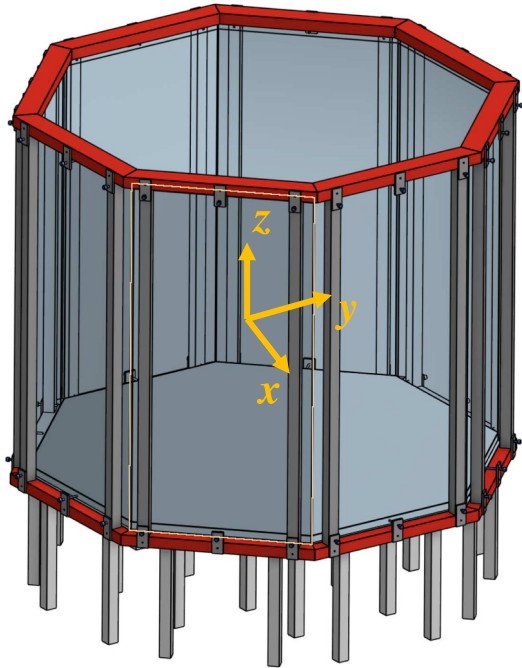


Particle settling at finite-Reynolds numbers



Brandt & Coletti (2022)

Particle settling at finite-Reynolds numbers



Non-turbulent region for initial particle settling

Large vertical extent of homogenous isotropic turbulence

Non-turbulent and wall-affected region where settled particles collect



Turbulence parameters:

$$Re_\lambda = 300$$

$$u_{rms} = 3 \text{ cm/s}$$

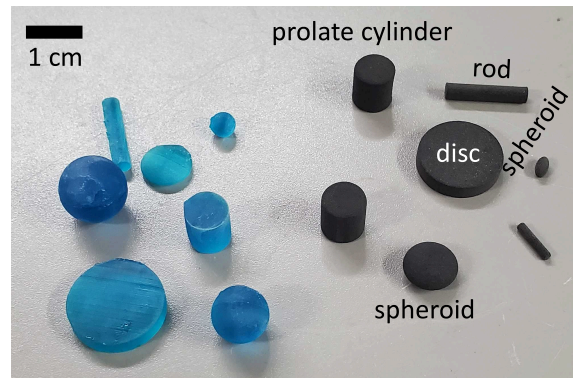
$$L_{int} = 10 \text{ cm}$$

$$T_{int} = 3 \text{ s}$$

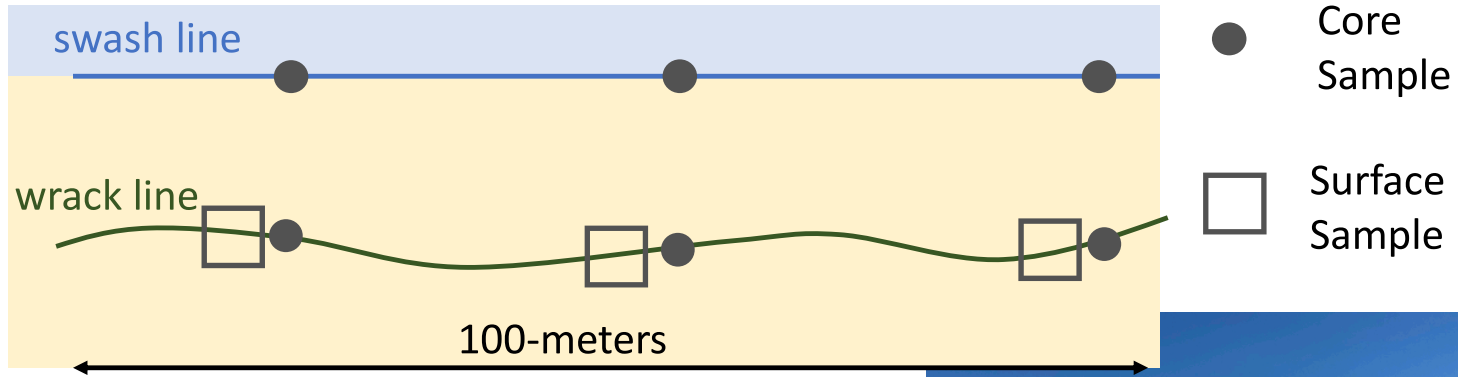
$$\langle \epsilon \rangle = 10^{-4} \text{ m}^2/\text{s}^{-3}$$

$$\eta_K = 0.3 \text{ mm}$$

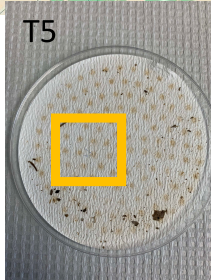
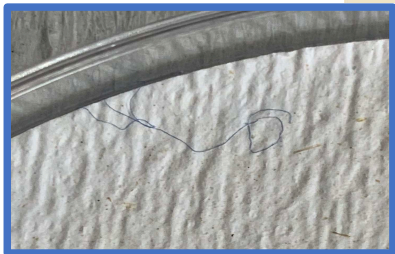
$$\tau_K = 0.1 \text{ s}$$



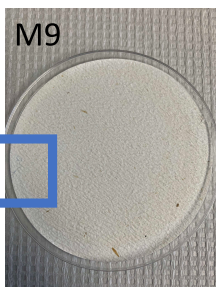
Microplastic beaching and swash burial



Michigan Sea Grant



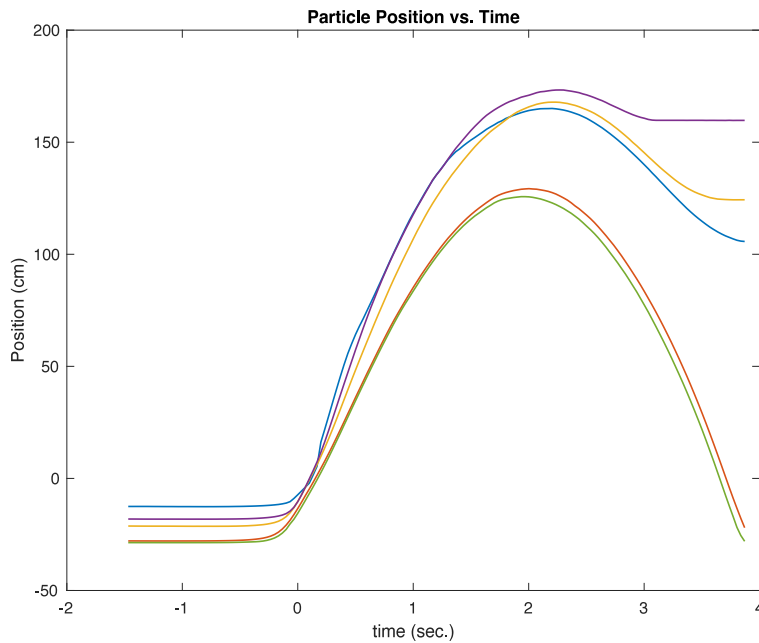
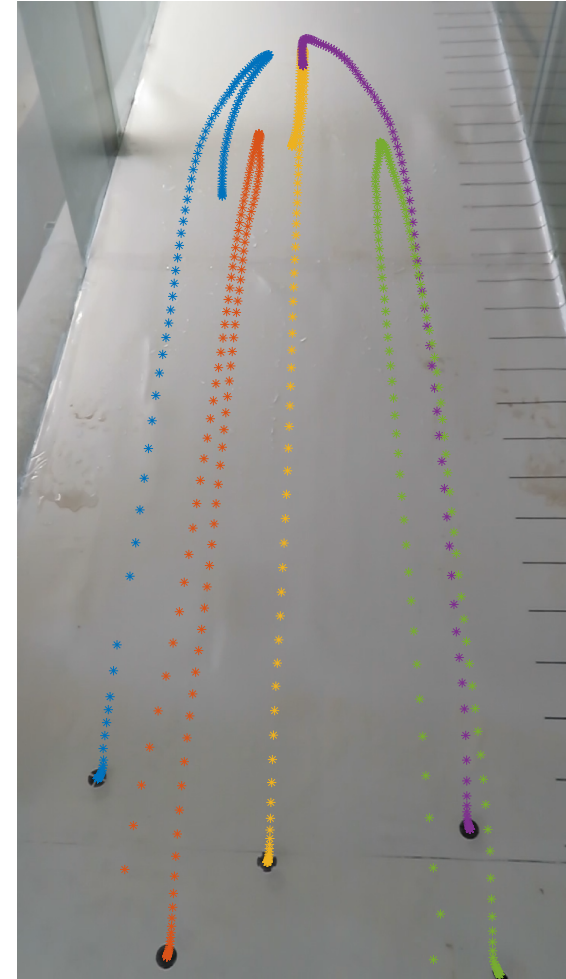
T5



M9



Microplastic beaching and swash burial



Acknowledgements



Michelle
DiBenedetto



Laura
Clark

Enhanced settling and dispersion of inertial particles in surface waves

Reference

DiBenedetto, Clark, Pujara (2022) *JFM* 936, A38



Ben Davidson
Microplastic beaching and swash burial



Joo Young Bang
Particle settling at finite Reynolds numbers



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